

PCT

WORLD INTELLECTUAL PROPERTY ORGANIZATION  
International Bureau

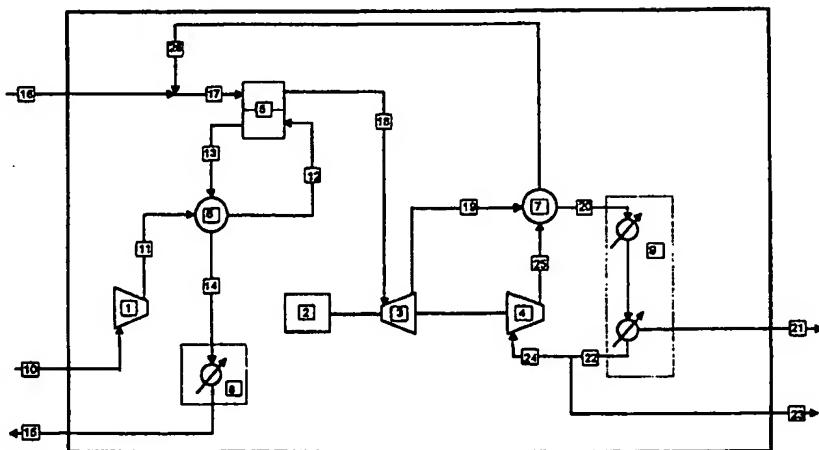


INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification 6 :		(11) International Publication Number:	WO 98/55394
C01B 13/02, B01D 53/22, 53/32, F23C 11/00	A1	(43) International Publication Date:	10 December 1998 (10.12.98)

(21) International Application Number:	PCT/NO97/00171	(81) Designated States: AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, ES, FI, GB, GE, HU, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, TJ, TM, TR, TT, UA, UG, US, UZ, VN, ARIPO patent (GH, KE, LS, MW, SD, SZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG).
(22) International Filing Date:	2 July 1997 (02.07.97)	
(30) Priority Data:	972631                    6 June 1997 (06.06.97)	NO
(71) Applicant (for all designated States except US):	NORSK HYDRO ASA [NO/NO]; N-0240 Oslo (NO).	
(72) Inventors; and		Published
(75) Inventors/Applicants (for US only):	ÅSEN, Knut, Ingvar [NO/NO]; Tiurv. 22, N-3940 Heistad (NO). SANDVOLD, Erik [NO/NO]; Skiferv. 31, N-3931 Porsgrunn (NO). LONGVA, Petter, Inge [NO/NO]; Voll Terrasse 21, N-1342 Jar (NO).	With international search report.
(74) Agent:	SUNDNES, Arne; Norsk Hydro ASA, N-0240 Oslo (NO).	

(54) Title: PROCESS FOR GENERATING POWER AND/OR HEAT COMPRISING A MIXED CONDUCTING MEMBRANE REACTOR



**FOR THE PURPOSES OF INFORMATION ONLY**

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AL	Albania	ES	Spain	LS	Lesotho	SI	Slovenia
AM	Armenia	FI	Finland	LT	Lithuania	SK	Slovakia
AT	Austria	FR	France	LU	Luxembourg	SN	Senegal
AU	Australia	GA	Gabon	LV	Latvia	SZ	Swaziland
AZ	Azerbaijan	GB	United Kingdom	MC	Monaco	TD	Chad
BA	Bosnia and Herzegovina	GE	Georgia	MD	Republic of Moldova	TG	Togo
BB	Barbados	GH	Ghana	MG	Madagascar	TJ	Tajikistan
BE	Belgium	GN	Guinea	MK	The former Yugoslav Republic of Macedonia	TM	Turkmenistan
BF	Burkina Faso	GR	Greece	ML	Mali	TR	Turkey
BG	Bulgaria	HU	Hungary	MN	Mongolia	TT	Trinidad and Tobago
BJ	Benin	IE	Ireland	MR	Mauritania	UA	Ukraine
BR	Brazil	IL	Israel	MW	Malawi	UG	Uganda
BY	Belarus	IS	Iceland	MX	Mexico	US	United States of America
CA	Canada	IT	Italy	NE	Niger	UZ	Uzbekistan
CF	Central African Republic	JP	Japan	NL	Netherlands	VN	Viet Nam
CG	Congo	KE	Kenya	NO	Norway	YU	Yugoslavia
CH	Switzerland	KG	Kyrgyzstan	NZ	New Zealand	ZW	Zimbabwe
CI	Côte d'Ivoire	KP	Democratic People's Republic of Korea	PL	Poland		
CM	Cameroon	KR	Republic of Korea	PT	Portugal		
CN	China	KZ	Kazakhstan	RO	Romania		
CU	Cuba	LC	Saint Lucia	RU	Russian Federation		
CZ	Czech Republic	LI	Liechtenstein	SD	Sudan		
DE	Germany	LK	Sri Lanka	SE	Sweden		
DK	Denmark	LR	Liberia	SG	Singapore		
EE	Estonia						

Process for generating power and/or heat comprising  
a mixed conducting membrane reactor.

The present invention relates to a process for generating heat and/or power comprising a membrane reactor where a fuel is oxidised and further comprising an improved method for reducing emissions of carbon dioxide and emission of oxides of nitrogen from said process.

Due to the environmental aspects of CO<sub>2</sub> and NO<sub>x</sub> and taxes on the emissions to the national authorities the possibilities for reducing the emissions of these compounds to the atmosphere from combustion processes, in particular from flue gas from gas turbines offshore, has been widely discussed.

Conventional combustion processes, used for carbon containing fuels and where the oxygen source is air, produce carbon dioxide concentrations of 3-15% in the exhaust gas dependent on the fuel and the applied combustion- and heat recovery process. The reason the concentration is this low is because air is made up of about 78% by volume of nitrogen.

Thus, a reduction in the emission of carbon dioxide makes it necessary to separate the carbon dioxide from the exhaust gas, or raise the concentration to levels suitable for use in different processes or for injection and deposition.

CO<sub>2</sub> can be removed from exhaust gas by means of several separation processes e.g. chemical active separation processes, physical absorption processes, adsorption by molecular sieves, membrane separation and cryogenic techniques. Chemical absorption by means of alkanol amines is considered as the most practical and economical method to separate CO<sub>2</sub> from power plant exhaust gas.

But this method does require heavy and voluminous equipment and will reduce the power output with about 10% or more. These known methods are however considered as not being very suited to practical implementation in a power generation process. In e.g. natural gas based power plants the fuel cost comprises a substantial part of the total cost of electric power. A high efficiency is therefore very important in order to reduce the cost of electric power.

In the mono ethanol amine (MEA) process CO<sub>2</sub> from the cooled power plant exhaust gas reacts with aqueous solution of MEA in an absorption tower. Most of the CO<sub>2</sub> is thus removed from the exhaust gas that is released to the atmosphere. MEA will be degraded and e.g. a 350 MW combined cycle power plant will produce about 4000 tons MEA degradation products per year which has to be destructed or stored.

In order to meet national NO<sub>x</sub> control requirements different methods can be used for instance burner modifications, applications of catalytic burners, steam additions or selective catalytic reduction (SCR) of the NO<sub>x</sub> in the exhaust gas. When air is used in combustion processes some of the nitrogen will be oxidised during the combustion to NO, NO<sub>2</sub> and N<sub>2</sub>O (referred to as thermal NO<sub>x</sub>). At least 80 -98% of the NO<sub>x</sub> formed arises from the said oxidation of nitrogen in air. The rest arises from oxidation of the nitrogen content in the fuel.

A method to both increase the concentration of CO<sub>2</sub> in an exhaust gas and to reduce the NO<sub>x</sub> formation is to add pure oxygen to the combustion process instead of air.

However, commercial air separation methods (cryogenic separation and PSA) will require 250 to 300 KWh/ton oxygen produced. Supplying oxygen e.g. to a gas turbine by this methods will decrease the net power output of the gas turbine cycle by at least 20%. The cost of producing oxygen in a cryogenic unit will increase

the cost of electric power substantially and may constitute as much as 50% of the cost of the electric power.

The main object of this invention was to arrive at a more efficient heat and power generating process comprising a combustion process which produce an exhaust gas with a high concentration of CO<sub>2</sub> and a low concentration of NO<sub>x</sub> that makes the exhaust gas stream suitable for direct use in different processes or for injection in a geological formation for long term deposition or for enhanced oil or natural gas recovery.

Another object of the invention was to supply oxygen to the combustion process which implies reduced energy demands compared to other known methods.

A further object was to utilise existing process streams in the power generation plant in obtaining improved oxygen supply to the combustion process.

The problem mentioned above concerning reduced fuel efficiency and high costs can partly be solved by application of mixed conducting membranes which is defined as a membrane made from material with both ion and electronic conductivity.

Such a membrane can be a mixed oxygen ion and electron conducting membrane, for instance capable of separating oxygen from oxygen-containing gaseous mixtures at 400 - 1300 °C. An oxygen partial pressure difference causes oxygen ions to be transported through the membrane by reduction of oxygen on the high oxygen partial pressure side (feed side) and oxidation of the oxygen ions to gas on the low oxygen partial pressure side (the permeate side). In the bulk of the membrane oxygen ions are transported by a diffusive process. Simultaneously the electrons flow from the permeate side back to the feed side of the membrane.

The application of these membranes is a rather new technique and is generally known from the European patent application 0658 367 A2 which describe separation of oxygen from air by means of a mixed conducting membrane which is integrated with a gas turbine system. Pure oxygen near atmospheric pressure or below and at high temperature is recovered from the permeate side of the conducting membrane. This, however, entail that the oxygen has to be cooled to below approximately 50°C and recompressed to required process pressure before being added to the oxidation reactor or burner in a combustion process.

The inventors then found to applicate a mixed oxygen ion and electron conducting membrane reactor, hereafter called a membrane reactor, to combine the supply of oxygen and burning of a fuel giving a hot gas mixture consisting of CO<sub>2</sub> and water and minor amounts of CO and H<sub>2</sub>.

The principle of the electropox process as described in European patent application 0 438 902 A3 could be adopted for this membrane burner or the principle of the electrochemical reactor described in US Patent 5,356,728. Complete combustion of the fuel in the membrane burner is, probably, not possible. However, minor amounts of unconverted partially oxidised fuel in the CO<sub>2</sub>-containing purge gas leaving the gas turbine process, can be oxidised separately in a small catalytic or non-catalytic combustion chamber by mixing the CO<sub>2</sub>-containing purge gas with an oxygen-containing gas or pure oxygen. The CO<sub>2</sub>-containing purge gas could also be injected to a geological formation without further treatment. If the CO<sub>2</sub>-containing exhaust gas is applied for enhanced oil recovery the nearly zero oxygen content in the exhaust gas would be an advantage.

Further the inventors found to applicate recycled carbon dioxide or a mixture of carbon dioxide and water, e.g. part of the exhaust gas, from the combustion process as a coolant in the membrane reactor. Carbon deposition on the second surface (the oxidation side) can be avoided by properly selection of catalyst

material and by properly adjusting the ratio between fuel and recycled CO<sub>2</sub> and H<sub>2</sub>O containing exhaust gas. By applying the membrane reactor oxygen could be recovered and reacted with a fuel without intermediate cooling and recompression of the oxygen as required in the European application 0658367. An additional advantage is that the operation pressure on the feed side of the membrane reactor can be lower or much lower than the operation pressure on the oxidation side of the membrane burner because the partial pressure of oxygen on the oxidation side will be less than about 10<sup>-15</sup> bar due to the oxidation reactions. This implies that oxygen can be supplied to a high pressure oxidation process without a first compression of air and the result of that is increased efficiency of the power production. In a conventional gas turbine power generator the compression of oxygen consumed in the combustion process constitute about 6 to 10% of the total power output of the process.

Thus the inventors surprisingly found that their method has the advantage of supplying oxygen to the combustion process with no loss in the efficiency of the power and/or heat generating plant. More surprisingly the method could increase the efficiency of a gas turbine power generation process compared to conventional gas turbine processes and at the same time produce an exhaust gas with nearly zero NO<sub>x</sub> and with a high concentration of CO<sub>2</sub>.

To obtain a sufficient high flux of oxygen through the membrane a rather high temperature is required (400 -1300 °C). On the air side of the membrane this can be accomplished by using a burner to increase the temperature for instance as disclosed in European patent application 0658 367 A2 . In order to avoid CO<sub>2</sub> in the air stream the air can be preheated by first heat exchanging with hot oxygen depleted air leaving the feed side of the membrane reactor and second in the membrane burner by heat exchanging with hot combusted fuel. The recycled CO<sub>2</sub> and H<sub>2</sub>O containing exhaust gas could be pre-heated in a recuperator and further preheated inside the membrane reactor.

Additional advantages of the improved heat and power generating process is reduced emissions of NO<sub>x</sub> due to the fact that very little nitrogen is present in the CO<sub>2</sub>-based combustion system. This will also allow for development of improved and more efficient gas turbine or combustion systems since NO<sub>x</sub>-control no longer is required. The higher specific heat capacity of CO<sub>2</sub> or a CO<sub>2</sub>/H<sub>2</sub>O-mixture than nitrogen will allow for development of more compact gas turbine systems and heat recovery systems, too.

A process for generation of heat/and/or power comprising a membrane reactor where fuel is oxidised according to the present invention, comprises that there is applied a membrane reactor being a mixed oxygen ion and electron conducting membrane reactor comprising a first surface (feed side) capable of reducing oxygen to oxygen ions and a second surface (oxidation side) capable of reacting oxygen ions with a carbon containing fuel.

A special feature of the invention is that the carbon containing fuel is mixed with recycled CO<sub>2</sub> and H<sub>2</sub>O containing exhaust gas before being supplied to the oxidation side of the membrane reactor.

A further embodiment of the invention is that a gas mixture leaving the combustion process is fed to a heat and/or power recovery system and that the thus cooled CO<sub>2</sub> containing gas mixture is compressed for further injection in an oil and gas reservoir for enhanced oil recovery or is compressed for injection to an geological formation.

Another feature of the invention is that air is heated before being supplied to the feed side of the membrane reactor at about atmospheric pressure.

The invention will be further explained and envisaged in the example and corresponding figures.

Figure 1 shows a combined power and heat generation process according to the invention and comprising a gas turbine cycle where part of the heat is recovered as mechanical or electrical power.

Figure 2 shows a heat generating process according to the invention operated at near atmospheric pressure.

Figure 1 shows a combined power and heat generating process comprising application of an air blower 1 to feed air to a membrane reactor 5 and a gas turbine system, (units 2, 3, 4, 7 and 9), integrated with the said membrane reactor and where the membrane reactor is applied instead of a conventional gas turbine combustor.

Air 10 is fed to heat exchanger 6 by means of blower 1. The hot air (stream 12) is then fed to a membrane unit 5 and oxygen is depleted giving a depleted air stream 13. Stream 13 is heat exchanged with the air stream 11 and heat can be further recovered in unit 8. The cooled nitrogen containing gas (stream 15) is discharged off. Recycled pressurised CO<sub>2</sub>-containing exhaust gas (stream 26) is mixed with fuel (stream 16) and the mixture (stream 17) is fed to the membrane unit 5 countercurrent to the air stream 12 and the fuel is reacted with oxygen on the membrane surface which is coated with an oxidation catalyst. The hot exhaust gas mixture (stream 18) is expanded in gas turbine expander 3, which is connected to an electrical power generator 2, and the resulting stream 19 is then heat exchanged in a recuperator 7 with recycled compressed exhaust gas (stream 25).

The exhaust gas stream 20 leaving recuperator 6 is fed to heat recovery unit 9 and condensed water is separated off as stream 21. Thereafter a part of the exhaust gas (stream 23) containing a high concentration of CO<sub>2</sub> is purged off.

The rest of the cooled exhaust gas stream 24 is compressed in compressor 4 and the resulting stream 25 is further pre-heated in recuperator 7 before being mixed with fuel (stream 16) and further added to the membrane reactor 5.

Figure 2 shows a heat generating process comprising application of a first air-based heat recovery system (units 1, 4, part of unit 3 and 6) which are integrated with a mixed conducting membrane unit 3 for supplying oxygen to a heat generating system (units 2, 5, 7, 8 and part of unit 3) comprising a nearly nitrogen free combustion process.

Air stream 9 is feed to heat exchanger 4 by means of blower 1. The hot air stream 11 is then fed to a membrane unit 3 and oxygen is depleted giving a depleted air stream 12 which is heat exchanged with the air stream 10. Heat can be further recovered in unit 6. The cooled nitrogen containing gas (stream 14) is discharged off. Recycled pressurised CO<sub>2</sub>- containing gas (stream 25) is mixed with fuel stream 15 and the mixture 16 is fed to the membrane unit countercurrent to the air stream 11 and the fuel is reacted with oxygen on the membrane surface which is coated with an oxidation catalyst. The hot gas mixture (stream 17) is fed to heat recovery system 7 and the resulting stream 18 is further heat exchanged in heat exchanger 5 with recycled gas (stream 24).

The gas stream 19 leaving heat exchanger 6 is fed to a heat recovery system 8 and condensed water 21 is separated off. Thereafter a part of the gas (stream 22) containing a high concentration of CO<sub>2</sub> is purged off.

The rest of the cooled gas stream 23 is recycled by means of blower 2 and the resulting stream 24 is further pre-heated in heat exchanger 7 before being mixed with fuel (stream 15) and further added to the membrane reactor 3.

#### Example 1

This example shows a power generation process as described in figure 1.

Air (10) is fed to heat exchanger 6 by means of a blower 1. The hot air (stream 12) is then fed to a membrane unit (5) and oxygen is depleted off giving a depleted air stream (13). The stream 13 is heat exchanged with the air stream 11 and can further be recovered in unit 8. The said gas contain less than 3% oxygen which allow for application in different chemical processes, e.g. for purging purposes. The air stream 12 was heated to about 500-1000°C in the membrane burner by heat exchanging with hot combusted fuel. Since no fuel is added to the air stream, 100% removal of CO<sub>2</sub> from the power plant is easily achieved.

Recycled pressurised CO<sub>2</sub>-containing exhaust gas (stream 26) is mixed with fuel (16) and the mixture is fed to the membrane unit (5) countercurrent to the air stream (12) and the fuel is reacted with oxygen on the membrane surface which is coated with an oxidation catalyst. The hot exhaust gas mixture at approximately 1000 to 1300 °C (stream 18) is expanded to near atmospheric pressure in the expander 3, which is connected to an electrical power generator 2, and the resulting stream (19) is then heat exchanged in a recuperator (7) with recycled compressed exhaust gas (stream 25).

The high heat capacity of carbon dioxide compared to nitrogen gives a higher temperature of the exhaust gas leaving the expander than in an air blown gas turbine system. Further the compression of recycled CO<sub>2</sub>-containing exhaust gas

will give a lower temperature than the compression of air to the same pressure. This will allow for application of a recuperator at pressure ratios up to at least 30.

Pre-heating of recycled compressed CO<sub>2</sub>-containing gas in a recuperator according to figure 1 will increase the efficiency of the power plant.

The exhaust gas stream 20, leaving recuperator 6 is fed to the heat recovery system 9 and condensed water stream 21 is separated off. Thereafter 3-20% of the exhaust gas (stream 23) containing a high concentration of CO<sub>2</sub> is purged off. The rest of the cooled exhaust gas stream 24 is compressed in compressor 4 and the resulting stream 25 is further pre-heated in recuperator 7 before being mixed with fuel (stream 16) and further added to the membrane reactor 5.

The CO<sub>2</sub>- containing stream 23 contains an insignificant amount of oxygen and the gas could thus be used for enhanced oil and natural gas recovery without further treatment. Stream 23 may contain minor amounts of partially oxidised components. If desired, these components could be oxidised in a catalytic reactor by addition of an oxidant.

In the process according to figure 1, 100% of the CO<sub>2</sub> generated in the combustion process, can be recovered as a high concentrated CO<sub>2</sub>-containing exhaust gas. The said exhaust gas, which is purged off, may contain an insignificant amount of oxygen and NO<sub>x</sub> and can further be applied for enhanced oil and natural gas recovery without further treatment, or the said gas may be injected to a geological formation for long term deposition.

Known methods are producing exhaust gases containing less than approximately 10% CO<sub>2</sub> which require application of an expensive, voluminous and heavy CO<sub>2</sub>- separation plant if e.g. deposition of CO<sub>2</sub> is essential. In order to remove NO<sub>x</sub> in these known processes a separate expensive catalytic system has to be installed. Compared to known methods comprising supply of pure oxygen to recycled

exhaust gas, the present invention will both increase the power efficiency of the plant and substantially reduce the cost of generation and supply of oxygen to the combustion process. Since no pure or concentrated oxygen streams are generated, serious risks due to handling of pure oxygen will be avoided. Air can be supplied to the combustion process at near atmospheric pressure. The mixed conducting membrane reactor provide a constant low partial pressure of oxygen on the oxidation side (combustion side) and allow oxygen to be transported from air at low pressure to the combustion process at high pressure saving compression of the oxygen used in the combustion process. Compared to conventional gas turbine power plants this way may allow for increased fuel efficiency.

### Example 2

This example shows a power generating process as described in figure 2.

Air (stream 9) is fed to heat exchanger 4 by means of blower 1. The hot air (stream 11) is then fed to a membrane unit 3 and oxygen is depleted giving a depleted air stream 12. Stream 12 is heat exchanged with the air stream 10 and heat can be further recovered in unit 6. Cooled oxygen depleted air (stream 14) is discharged off. The said gas may contain less than 3 % oxygen which allow for application in different chemical processes, e.g. for purging purposes.

The air stream 11 can be heated to about 400 - 1000 °C in the membrane burner by heat exchanging with hot combusted fuel. Since no fuel is added to the air stream, 100% removal of CO<sub>2</sub> from the heat generating plant is easily achieved.

Recycled pressurised CO<sub>2</sub> - containing gas (stream 25) is mixed with fuel (stream 15) and the mixture (stream 16) is fed to the membrane unit 3 countercurrent to the air stream 11 and the fuel is reacted with oxygen on the

membrane surface which is coated with an oxidation catalyst. The hot gas mixture at approximately 500 to 1300 °C (stream 17) is fed to heat recovery system 7 and the resulting stream 18 is further heat exchanged in heat exchanger 5 with recycled gas (stream 24).

The gas stream 19, leaving heat exchanger 6 is fed to a heat recovery system 8 and condensed water stream 21 is separated off. Thereafter 3 to 20% of the gas (stream 22) containing a high concentration of CO<sub>2</sub> is purged off.

The rest of the cooled gas stream 23 is recycled by means of a blower 2 and the resulting stream 24 is further pre-heated in heat exchanger 7 before being mixed with fuel (stream 15) and further added to the membrane reactor 3.

The CO<sub>2</sub>-containing stream 23 contains a not significant amount of oxygen and the gas could thus be used for enhanced oil and natural gas recovery without further treatment or it can be injected to a geological formation for long term deposition or it can be applied in different chemical processes.

Stream 22 may contain minor amounts of partially oxidised components. If desirable these components could be oxidised in a catalytic reactor by addition of an oxidant.

In the process according to figure 2, 100% of the CO<sub>2</sub> generated in the combustion processes, can be recovered as a high concentrated CO<sub>2</sub>-containing gas at atmospheric pressure. The said gas, containing a not significant amount of oxygen or NO<sub>x</sub>, may be injected to a geological formation for long term deposition. The process according to figure 2 can be applied for generation of heat in different chemical processes where removal of CO<sub>2</sub> is essential and could substantially reduce the cost of such removal compared to other known methods. The method saves NO<sub>x</sub>-reduction equipments, too. The method according to the invention could e.g. be applied in processes comprising units like column

reboilers, fractionating-column feed preheaters, reactor-feed preheaters, steam boilers and heated reactors.

The fuel added to the process is natural gas, methanol, synthesis gas comprising hydrogen and carbon monoxide, refinery fuel gas containing mixed hydrocarbons or other combustible gas mixtures.

By the present invention the inventors has arrived at a flexible power and/or heat generation process comprising an improved method for reducing the emissions of CO<sub>2</sub> and oxides of nitrogen to the atmosphere from the exhaust gas by generation of an exhaust gas containing a high concentration of carbon dioxide and a not significant concentration of nitrogen oxides. The exhaust gas is suitable for direct use in different processes or for injection and deposition or for enhanced oil and natural gas recovery. Exhaust gas consisting of more than 95% CO<sub>2</sub> can be generated without significant loss in the efficiency of the power or heat generation process.

This is obtained by application of a mixed oxygen ion and electron conducting membrane reactor instead of a conventional burner or combuster. Further the inventors found to applicate recycled carbon dioxide or a mixture of carbon dioxide and water, e.g. part of the exhaust gas, from the combustion process as a coolant in membrane reactor. Carbon deposition on the second surface (the oxidation side) can be avoided by properly selection of catalyst material and by properly adjusting the ratio between fuel and recycled CO<sub>2</sub> and H<sub>2</sub>O containing exhaust gas.

By applying the membrane reactor oxygen could be recovered and reacted with a fuel without intermediate cooling and recompression of the oxygen. An additional advantage is that the operation pressure on the feed side of the membrane reactor can be lower or much lower than the operation pressure on the oxidation side of the membrane burner because the partial pressure of oxygen on the

oxidation side will be very low due to the oxidation reactions. This implies that oxygen can be supplied to a high pressure oxidation process without a first compression of air and the result of that is increased efficiency of the power and heat generation compared to other known methods.

The oxygen depleted air leaving the feed side of the membrane reactor contains less than 3% oxygen and no combustion products, which allow for application in different chemical processes, e.g. for purging purposes.

The described application of mixed conductive membranes can in principle be used in the same way for several types of power or heat generation processes e.g. in Combined Cycle Power Plants or in Integrated Gasification and Combined Cycle power plants or in any processes comprising combustion of a fuel.

Claims

1. A process for generation of heat and/or power comprising a membrane reactor where a fuel is oxidised and further comprising an improved method for reducing emissions of carbon dioxide and emission of oxides of nitrogen from the said process,  
characterised in that  
there is applied a membrane reactor being a mixed oxygen ion and electron conducting membrane reactor comprising a first surface (feed side) capable of reducing oxygen to oxygen ions and a second surface (oxidation side) capable of reacting oxygen ions with a carbon containing fuel.
2. Process according to claim 1,  
characterised in that  
the carbon containing fuel is mixed with recycled CO<sub>2</sub> and H<sub>2</sub>O containing exhaust gas before being supplied to the oxidation side of the membrane reactor.
3. Process according to claim 1,  
characterised in that  
a gas mixture leaving the combustion process is fed to a heat and/or power recovery system and that the thus cooled CO<sub>2</sub> containing gas mixture is compressed for further injection in an oil and gas reservoir for enhanced oil recovery or is compressed for injection to an geological formation.
4. Process according to claim 1,  
characterised in that  
air is heated before being supplied to the feed side of the membrane reactor at about atmospheric pressure.

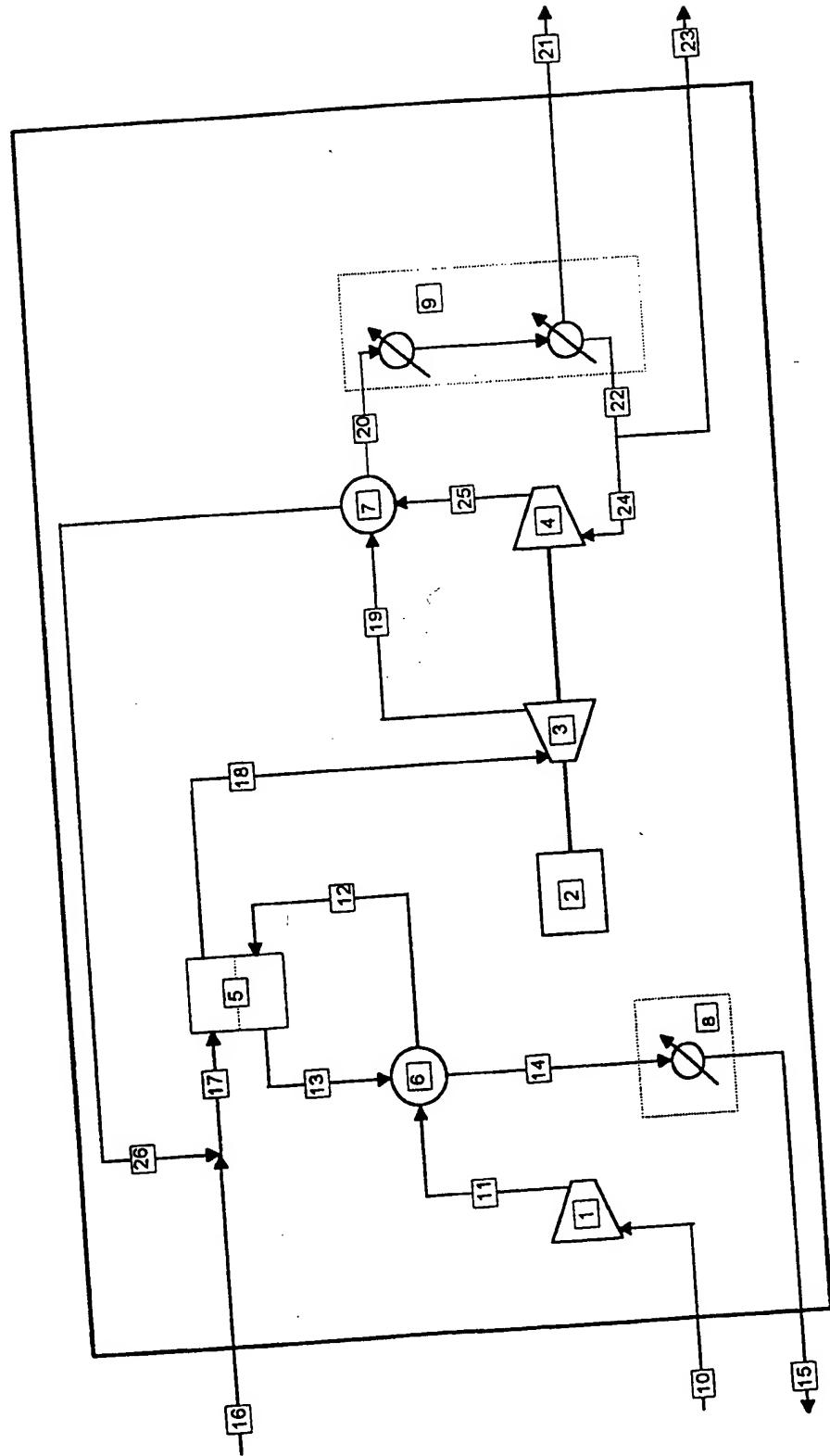


Fig. 1

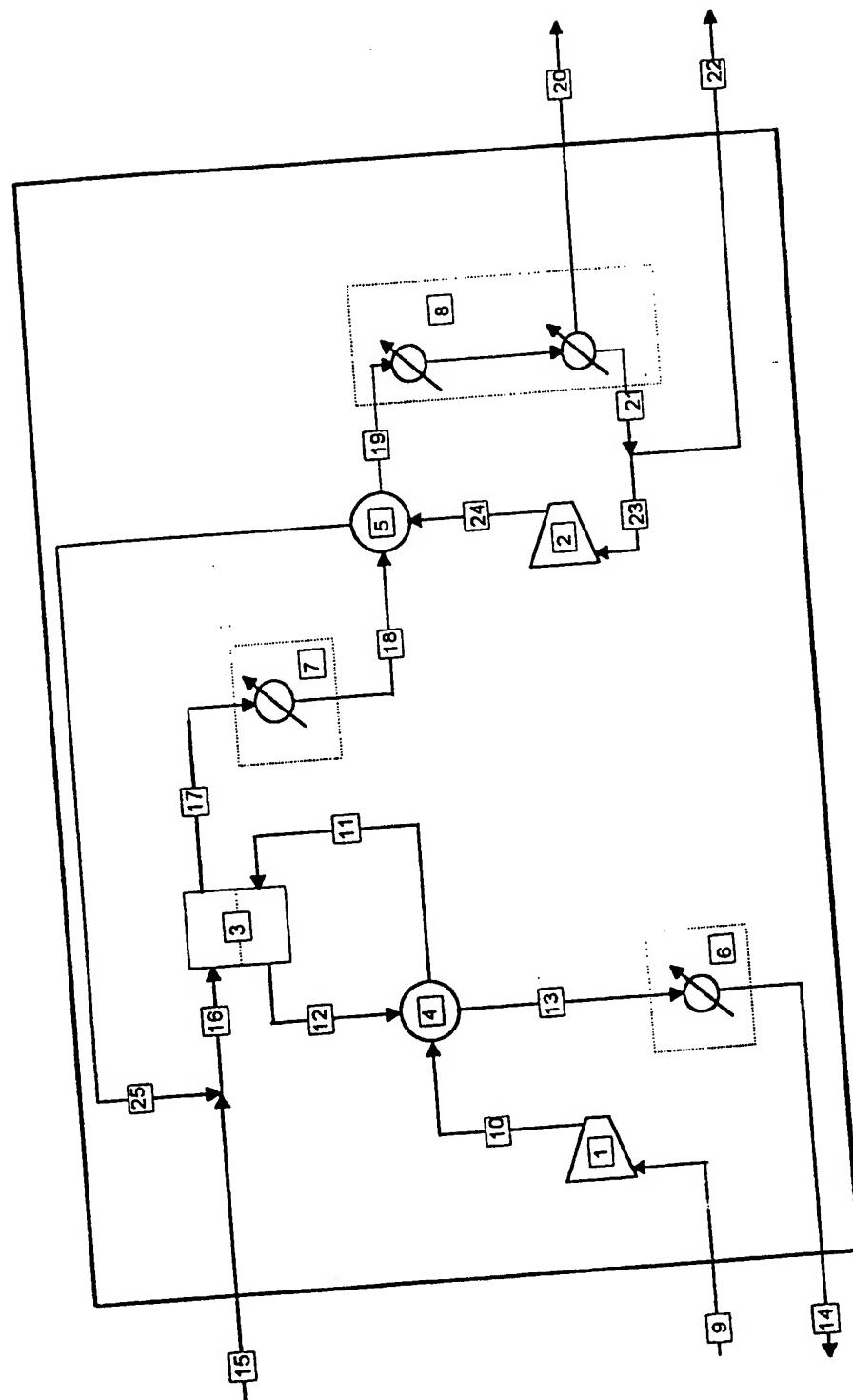


Fig. 2

1  
INTERNATIONAL SEARCH REPORT

International application No.  
PCT/NO 97/00171

## A. CLASSIFICATION OF SUBJECT MATTER

IPC6: C01B 13/02, B01D 53/22, B01D 53/32, F23C 11/00  
According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC6: C01B, B01D, F23C

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

SE,DK,FI,NO classes as above

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

EPODOC, WPI

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P,X	EP 0778069 A1 (PRAXAIR TECHNOLOGY, INC.), 11 June 1997 (11.06.97) --	1-4
E,X	WO 9741060 A1 (ELTRON RESEARCH, INC.), 6 November 1997 (06.11.97), page 2, line 29 - line 37; page 3, line 1 - line 2; page 7, line 23 - line 30, page 9, line 23 - line 37; page 10, line 1 - line 31; page 11, line 1 - line 37; page 12, line 1 - line 5 --	1-4
X	EP 0399833 A1 (THE STANDARD OIL COMPANY), 28 November 1990 (28.11.90) --	1-4

Further documents are listed in the continuation of Box C.

See patent family annex.

- \* Special categories of cited documents:
- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier document but published on or after the international filing date
- "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the international filing date but later than the priority date claimed

- "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- "X" document of particular relevance: the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- "Y" document of particular relevance: the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
- "&" document member of the same patent family

Date of the actual completion of the international search

Date of mailing of the international search report

06 -04- 1998

1 April 1998  
Name and mailing address of the ISA:  
Swedish Patent Office  
Box 5055, S-102 42 STOCKHOLM  
Facsimile No. + 46 8 666 02 86

Authorized officer

Marianne Bratsberg  
Telephone No. + 46 8 782 25 00

## INTERNATIONAL SEARCH REPORT

2

International application No.  
PCT/NO 97/00171

## C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages.	Relevant to claim No.
A	EP 0211523 A1 (HUMPHREYS & GLASGOW LIMITED), 25 February 1987 (25.02.87) --	1-4
A	EP 0658367 A2 (AIR PRODUCTS AND CHEMICALS, INC.), 21 June 1995 (21.06.95) -----	1-4

**INTERNATIONAL SEARCH REPORT**  
Information on patent family members

International application No.  
PCT/NO 97/00171

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
EP 0778069 A1	11/06/97	AU 7413196 A CA 2192014 A JP 9175802 A PL 317307 A	12/06/97 06/06/97 08/07/97 09/06/97
WO 9741060 A1	06/11/97	AU 6979196 A	19/11/97
EP 0399833 A1	28/11/90	AT 137421 T AU 5596290 A CA 2017243 A CN 1028493 B CN 1048169 A DE 69026752 D,T EP 0673675 A JP 3101833 A US 5306411 A US 5591315 A US 5693212 A US 5714091 A AT 152859 T AU 6838290 A CA 2032994 A DE 69030651 D,T EP 0438902 A,B EP 0766330 A ES 2100877 T JP 6056428 A NZ 236632 A	15/05/96 29/11/90 25/11/90 24/05/95 02/01/91 14/11/96 27/09/95 26/04/91 26/04/94 07/01/97 02/12/97 03/02/98 15/05/97 04/07/91 28/06/91 21/08/97 31/07/91 02/04/97 01/07/97 01/03/94 26/07/94
EP 0211523 A1	25/02/87	NONE	
EP 0658367 A2	21/06/95	US 5516359 A US 5565017 A	14/05/96 15/10/96